

I HAVE A NITROGEN STANDARD,
SO WHICH TECHNOLOGY
SHOULD I USE?

PERFORMANCE WASTEWATER SOLUTIONS

TN Design Parameters

- **Influent Concentration**

- USEPA indicates a range of influent TKN from 26 to 75 mg/l while sampling of single house systems has found TKN levels of up to 120 mg/l - some states have a design requirement of 100 mg/l for on-site systems

- **Influent source**

- Offices & schools high ammonia – low organics
- Campsites & holiday homes – seasonal use - long periods of no flow
- Restaurants – high BOD & FOG
- Commercial / Industrial – inhibitory substances
- Phased construction – potential carbon deficiency

TN Design Parameters

- **Project Design**

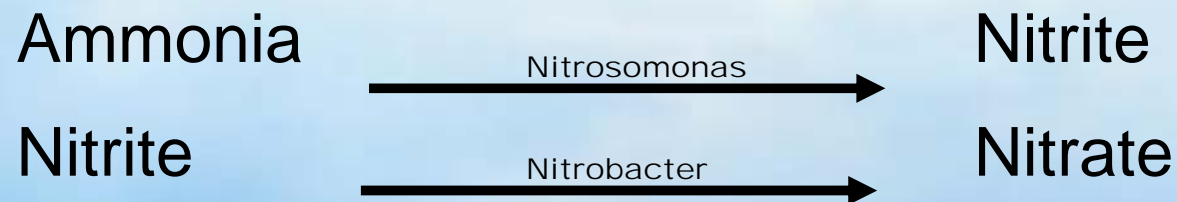
- Permit requirements – % reduction or mg/l, grab or composite sample – absolute spot, average or %ile treatment standards
- Design max daily flow & peak hourly flows – equalization tank
- Consider the complexity of O&M and who will manage
- Footprint, Sludge, Visual impact, Noise & Odor

- **Process Design**

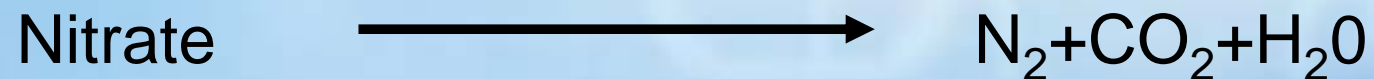
- Need to remove the BOD load first to allow the nitrifiers to dominate
- Sufficient Hydraulic retention time & oxygen to nitrify the wastewater
- Temperature – low <10 C affects biological activity, high requires a greater oxygen input
- Alkalinity, 7.14 mg consumed per mg ammonia removed (recirculation will recover half alkalinity lost)
- Sufficient carbon to denitrify - 2.72 mg BOD5 are required per mg of NO₃-N removed
- Anoxic tank to reduce DO to < 0.5 mg/l and allow denitrifying bacteria sufficient hydraulic retention time

Nitrogen Reduction

– Nitrification process - aerobic



– Denitrification process - anoxic

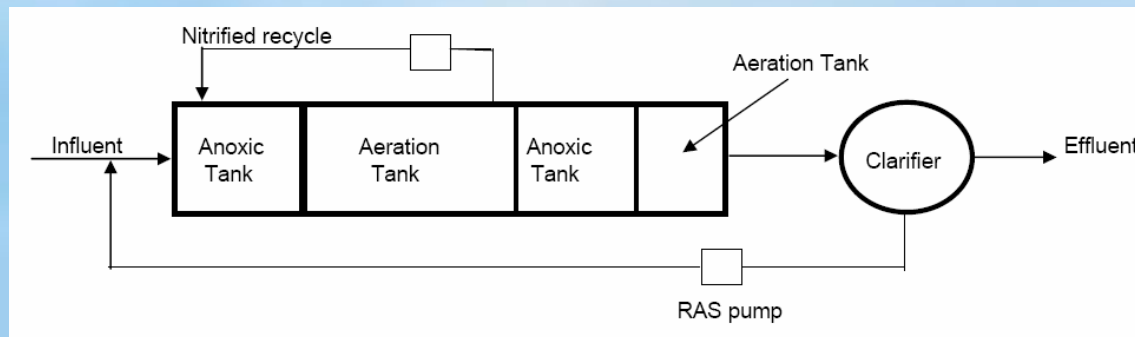
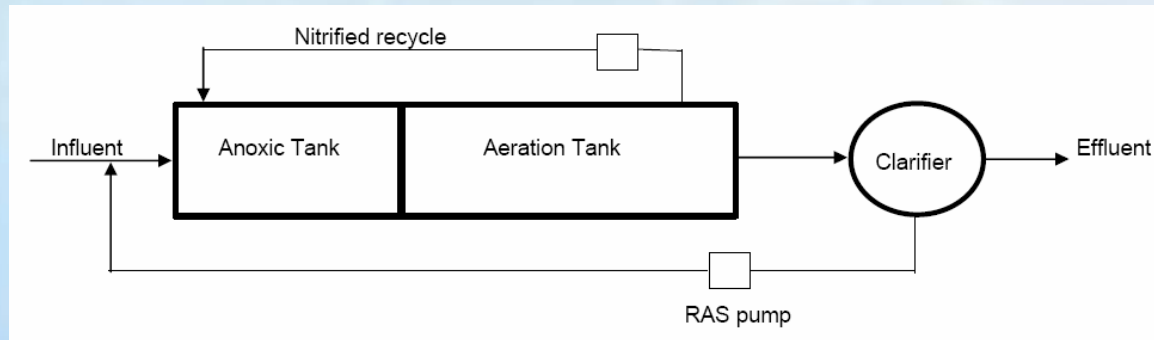


Suspended Growth Activated Sludge (ATUs)

Recirculation

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Suspended growth activated sludge



- BOD reduction and nitrification in aerated reactor(s) with the nitrified effluent recirculated to an anoxic reactor typically at rates of up to 400% of the influent flowrate

Suspended growth activated sludge using recirculation

- **Advantages include**

- Relatively simple and cost effective
- No requirement for supplemental carbon addition
- Recirculation allows recovery of alkalinity

- **Limitations**

- Carbon source is dependant on the influent (variable @ lower flows)
- Relatively large tank sizes required to maintain hydraulic retention time
- High strength TKN or tight permit standards requiring recirculation $> 4-6 Q$ can become limiting
- Recirculation only provides a % reduction of the influent load
- Equalization tank required to maintain the nitrifiers in the aeration stage
- Poor performance for intermittent flows
- Pump limitations for low flows
- Reliance on a clarifier

Sequencing Batch Reactor (SBR)

- The influent is batched and aeration and settlement is undertaken in the same tank
- Nitrogen reduction by increasing aeration for nitrification and adding an anoxic phase onto the batching cycle by turning the air off
- Effectively handles varying flows

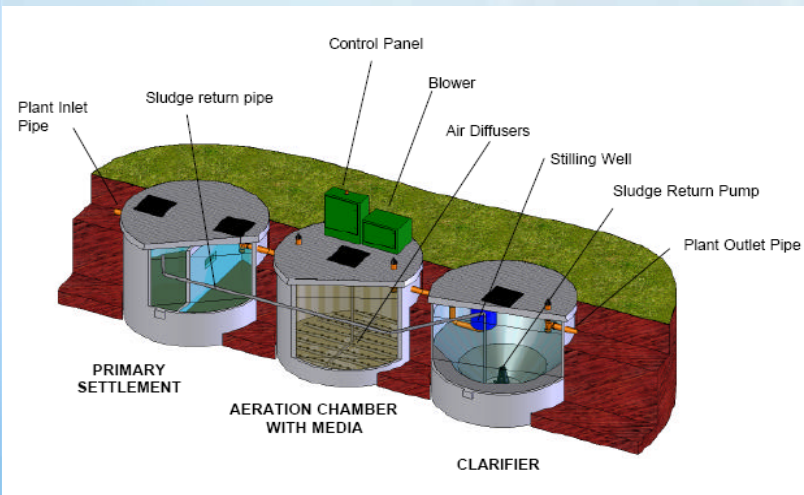


Fixed Film / Attached Growth Technologies

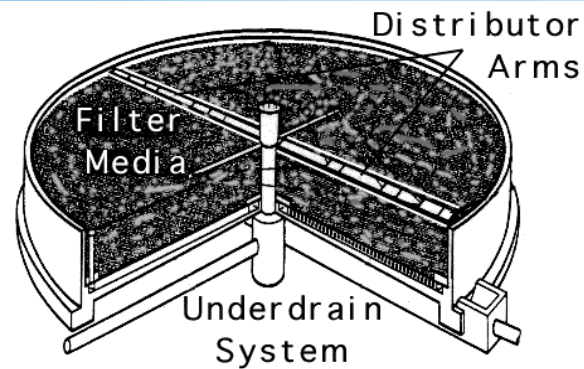
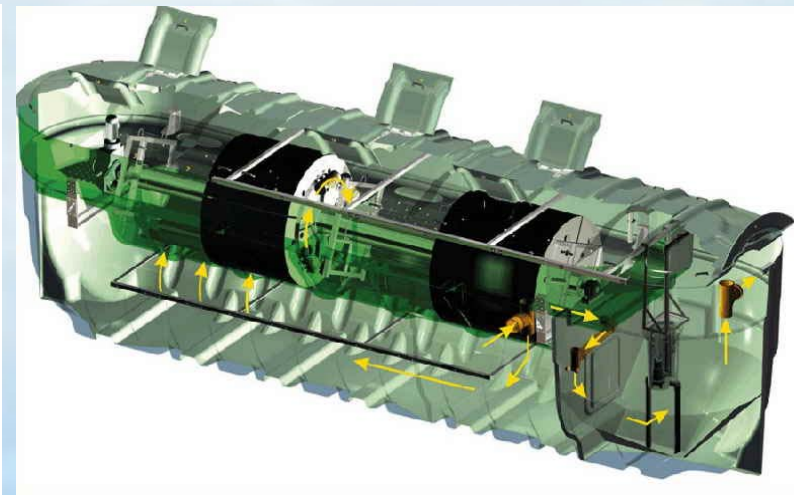
Post Anoxic Carbon Dosing

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MBBR

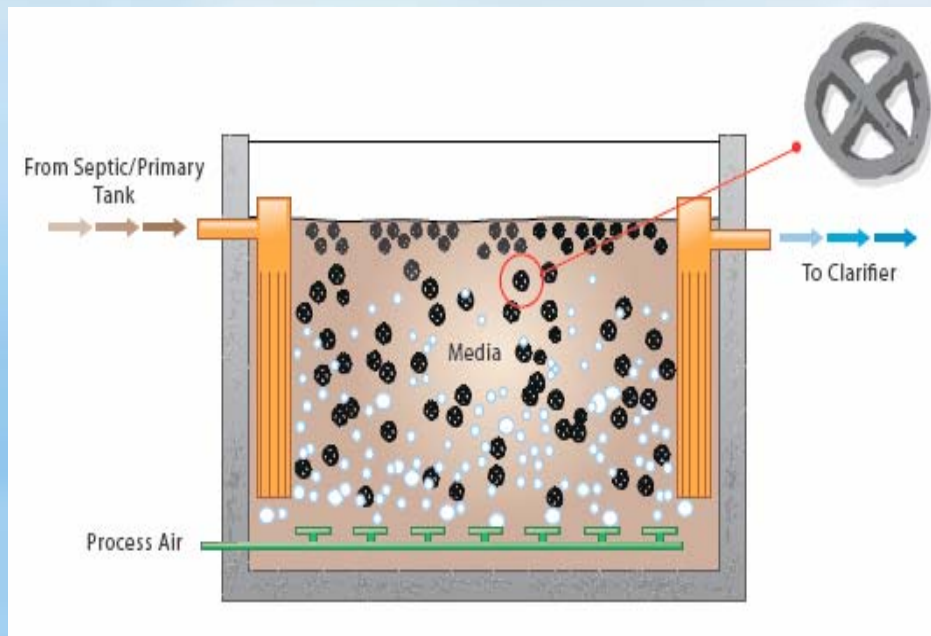


RBC



Trickling Filter

MBBR



- **MBBR - Plastic media provides an extended surface area for bacteria**
- **Less risk of nitrifiers being washed out**
- **Does not require return activated sludge systems**
- **Sludge sloughs off and settles in clarifier**

Treatment Performance

Parameters	Typical Values
BOD ₅	<15 mg/l
TSS	<20 mg/l
Ammonia	<5 mg/l ¹
Total Nitrogen	< 10 mg/l ²
Total Nitrogen	< 7.5 mg/l ³
Phosphorus	<1 mg/l ⁴

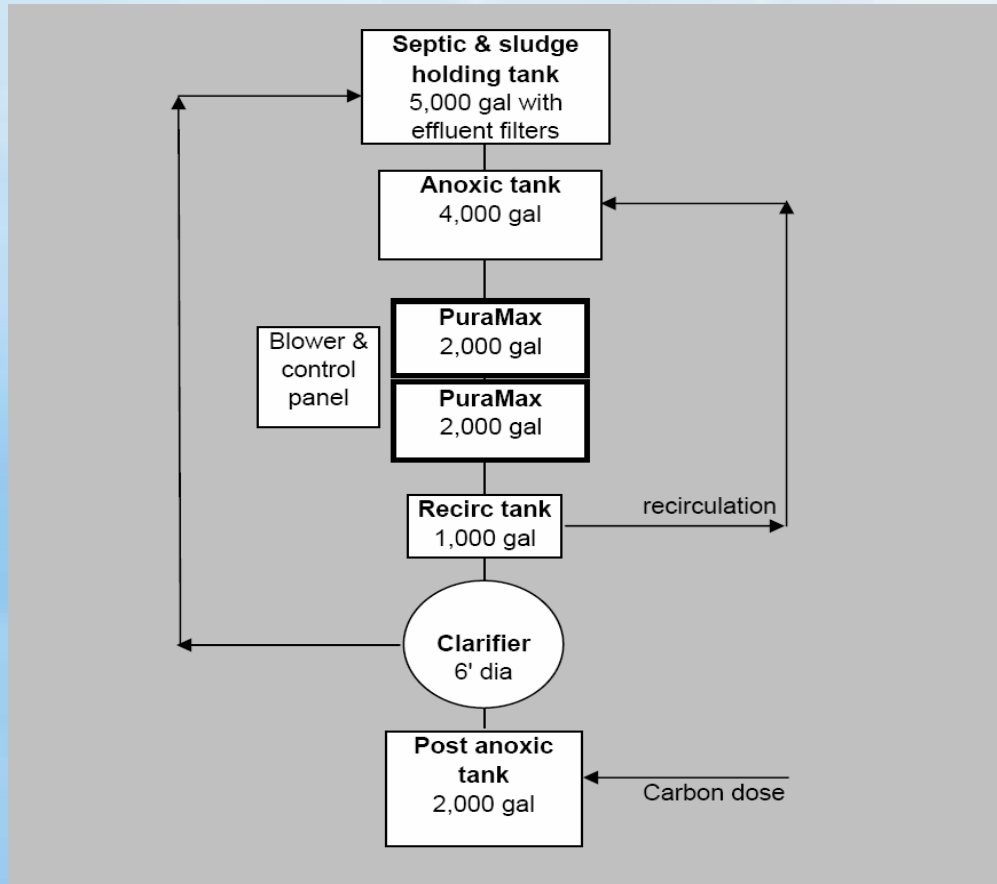
¹ Ammonia reduction design – decrease loading rate on media – two stage aeration to allow specialization of nitrifiers

² With recirculation where influent is <50 mg/l

³ With recirculation and a post anoxic reactor

⁴ With a chemical dosing system

Recirculation & post Anoxic Denitrification



BOD & TSS reduction

BOD reduction

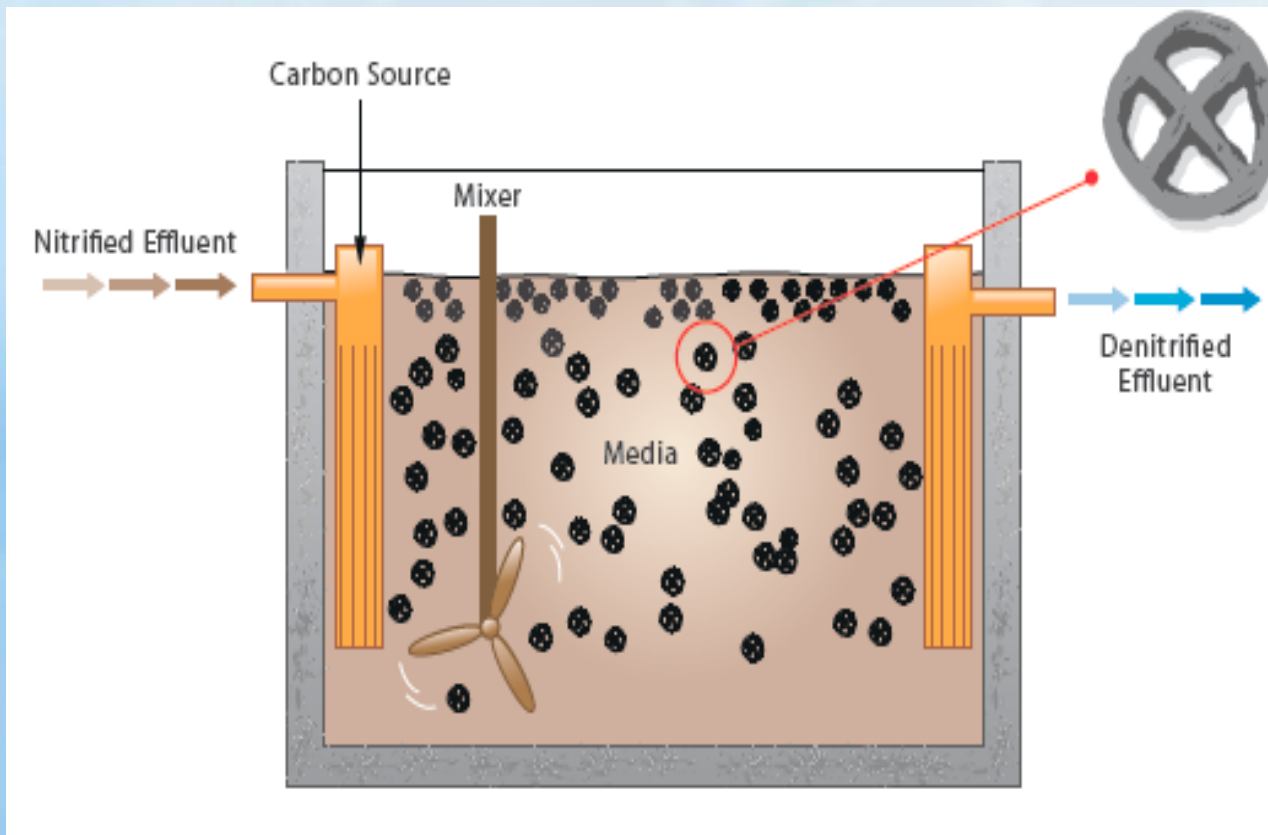
Nitrification

Denitrification ↑

Solids removal

Denitrification

Post Anoxic Denitrification



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Post anoxic MBBR systems

- **Advantages include**

- The carbon source is adjustable
- Resilience to shock loads as the nitrifiers are retained on the media
- Performs better than suspended growth activated sludge systems for intermittent flows and low carbon strength influents
- Small aeration reactor volumes for nitrification
- Ease of operation compared to suspended growth activated sludge systems as there is no RAS system

- **Limitations**

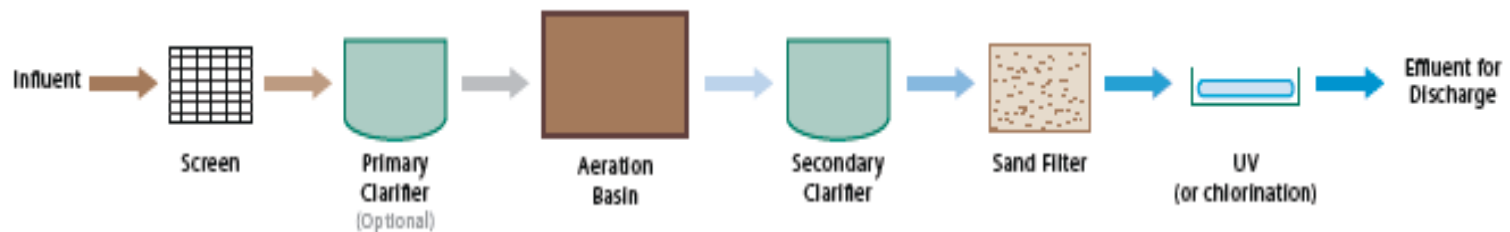
- For on-site systems a non-toxic carbon source would be required
- The carbon dose needs to be flow proportional to control the effluent BOD levels
- Alkalinity is not recovered as recirculation is not provided
- A post anoxic reactor may require re-oxygenation of the effluent where discharging to a surface water

Membrane Bioreactor

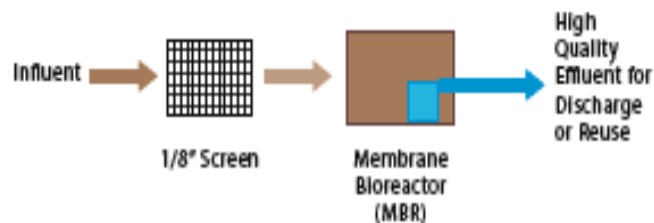
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Membranes compared to traditional Activated Sludge processes

Conventional Treatment Process



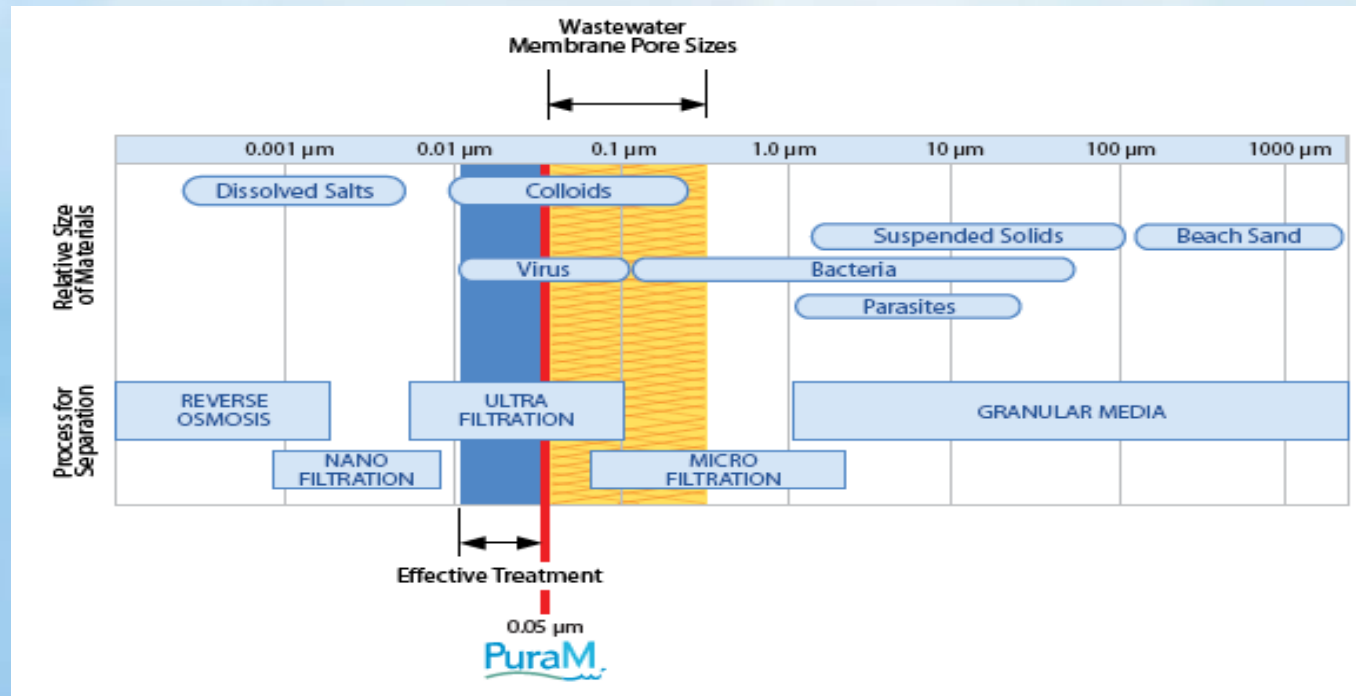
PuraM MBR Process



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Membrane Pore Sizes

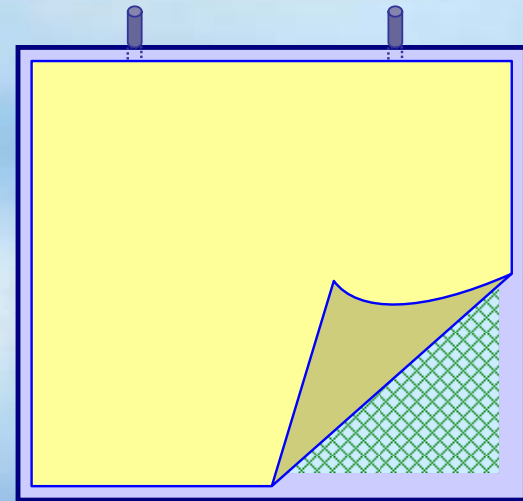
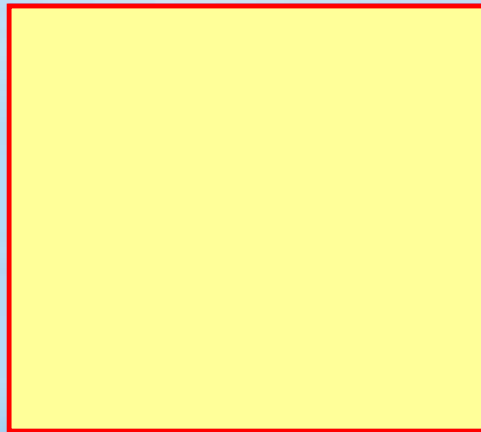
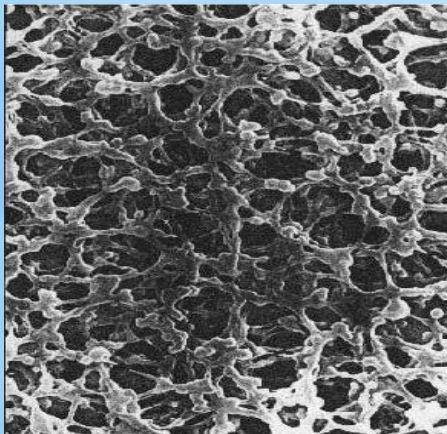
- Wastewater treatment in the micro & ultra filtration range
- Biofilm increases filtration capacity



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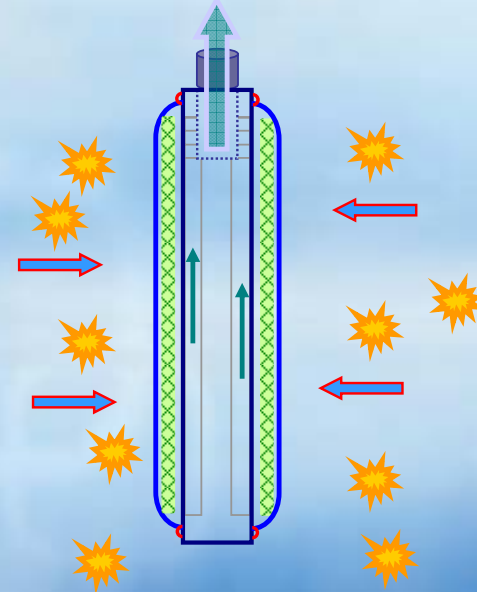
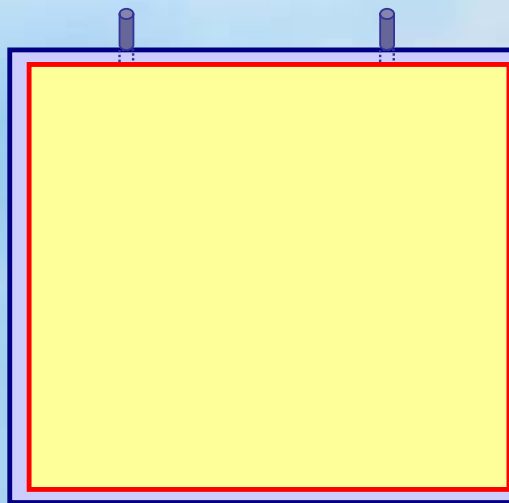
PLATE DESIGN

- Polysulphone membrane
- Plastic plate with spacer fabric
- Membrane ultrasonically welded to plate

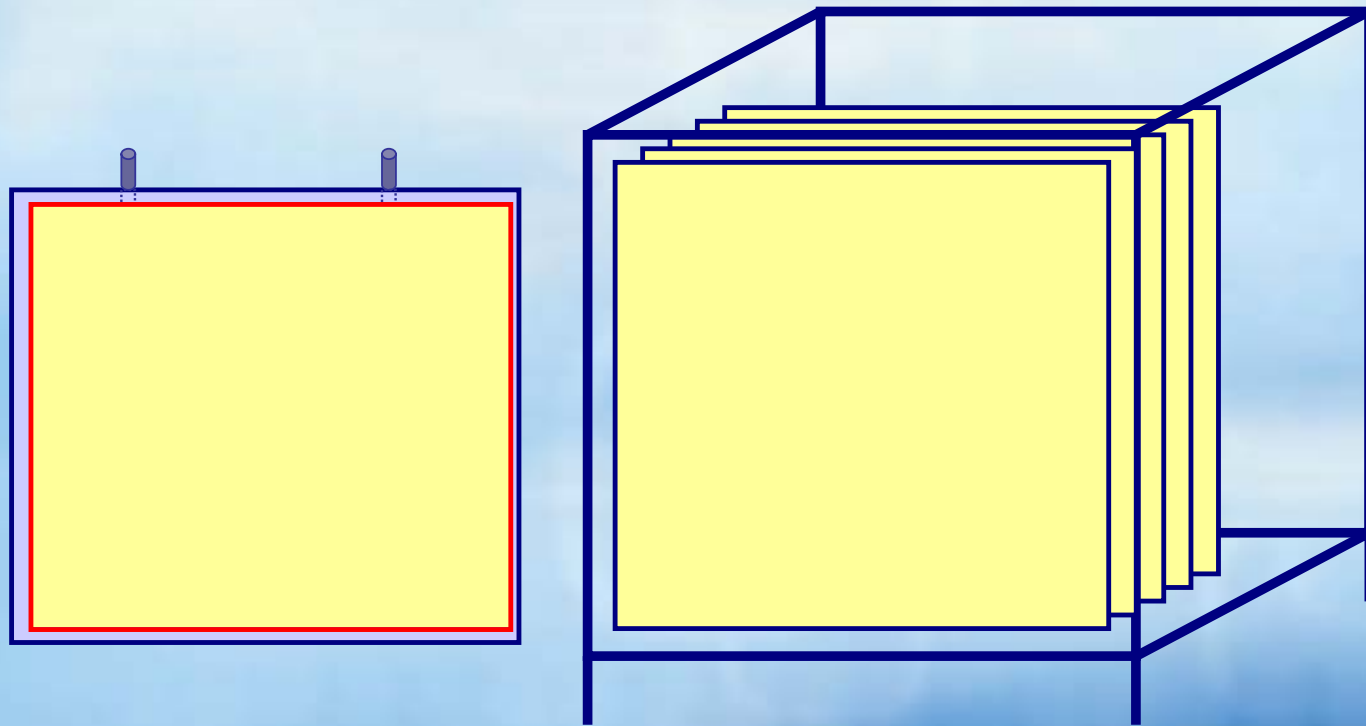


Membrane Operation

- **Outside to in flow**
- **Membrane provides absolute barrier**
 - Reduces affect of flow variation
 - Allows increased MLSS

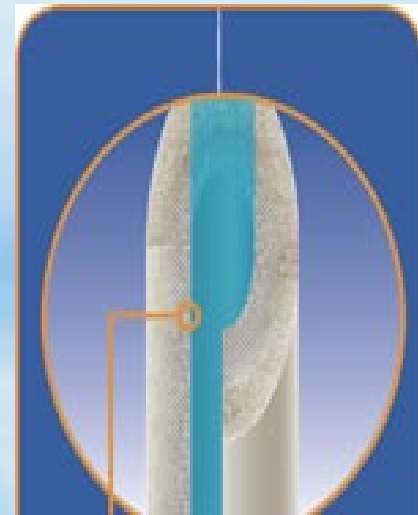
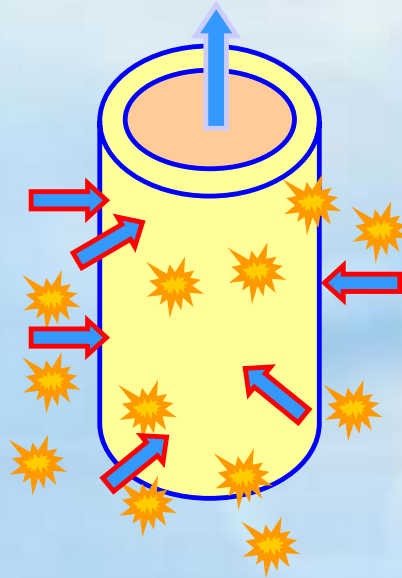


PuraM – Cassette



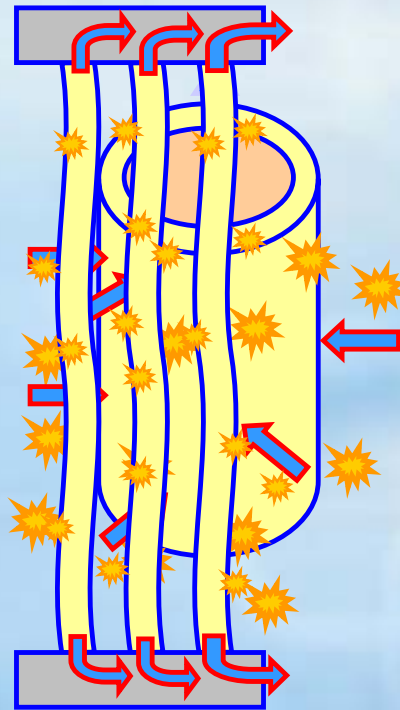
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Hollow Fiber Membrane System



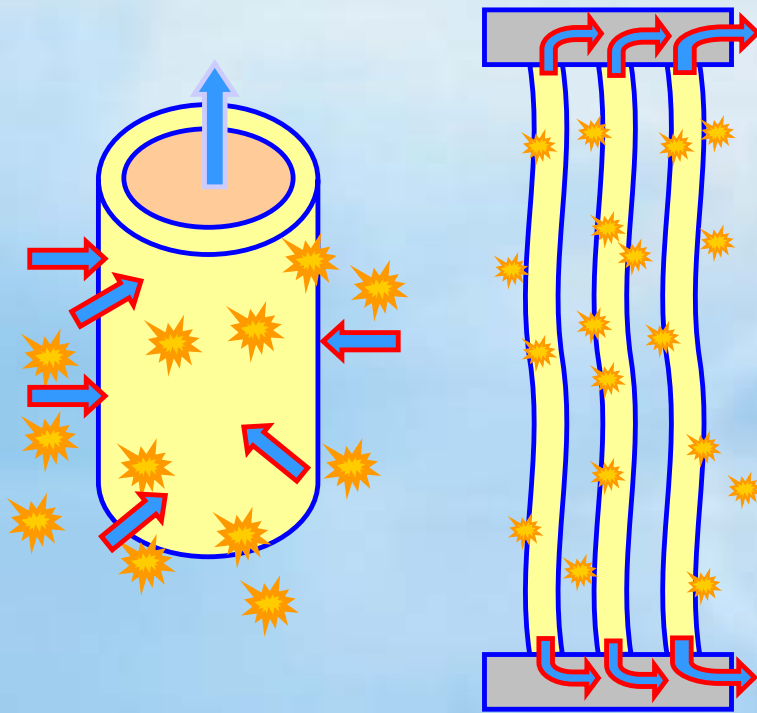
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Hollow Fiber Membrane System



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Hollow Fiber Membrane System



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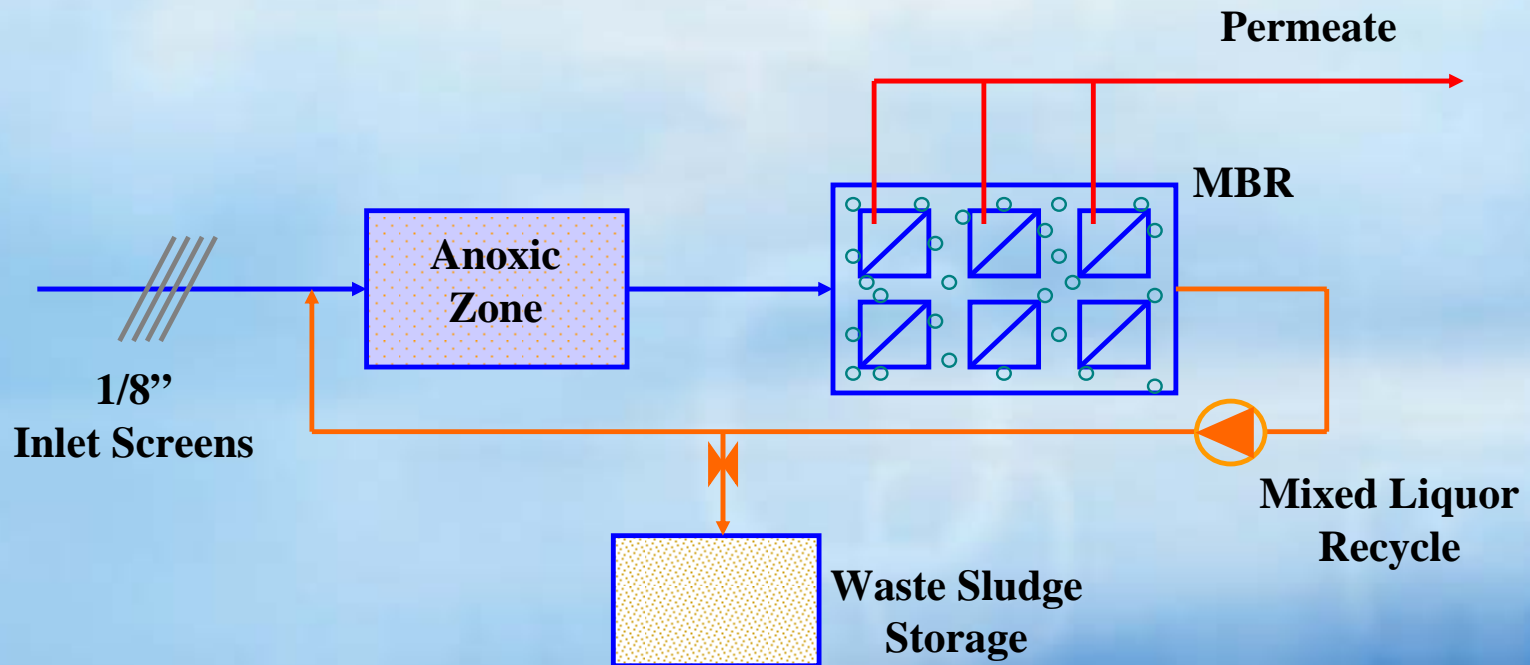
Membrane Selection

- Plate or Hollow Fibre?

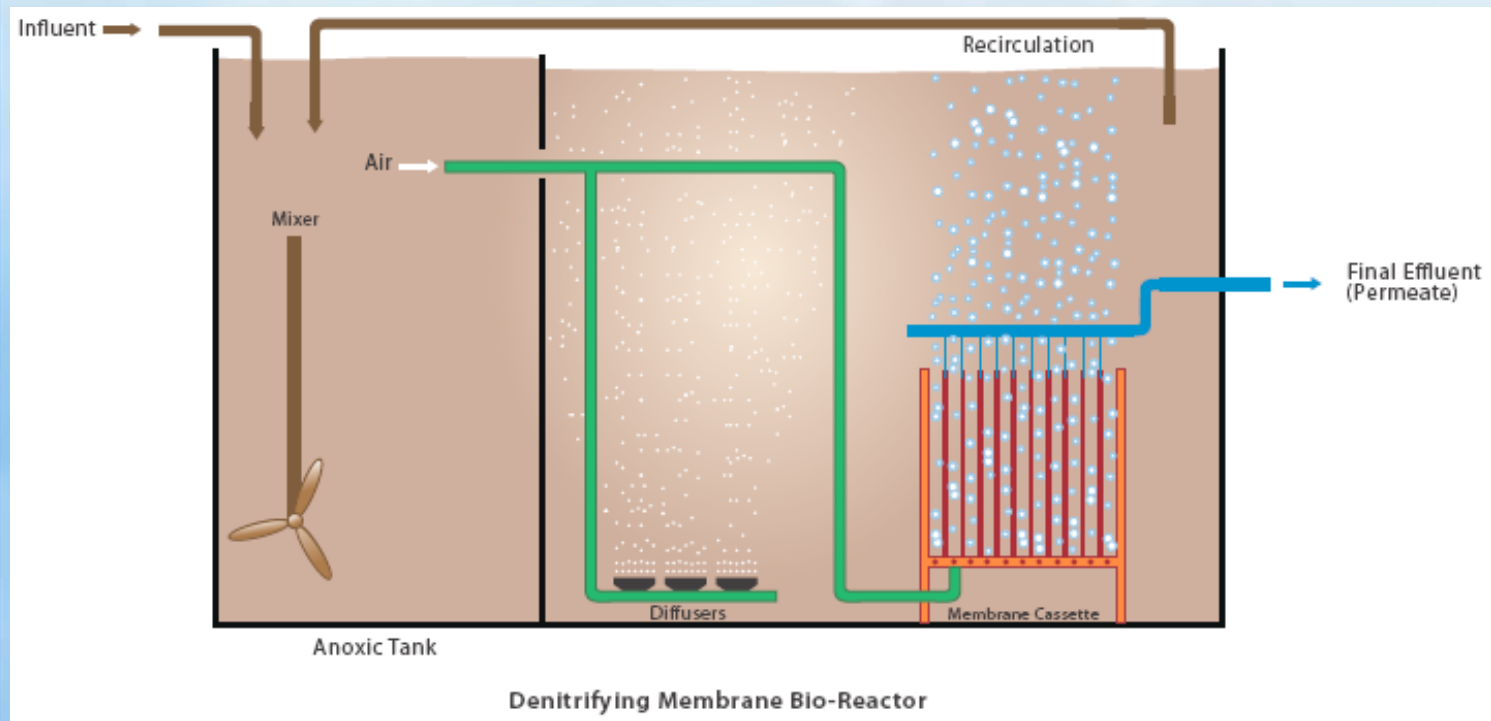
	Plate	Hollow Fibre
Footprint	Very Good	Better
Screening	1/8 inch	up to 1/32 inch
O&M	Relatively simple	More Complex
Air requirement	High	High - Medium
Membrane cleaning	Infrequent 6 to 18 months	Regular (backpulse / chemicals daily)
Traditional Suitability	Small flows < 1 million gpd	High flows > 150,000 gpd

Denitrification by recirculation

Design for TN removal < 10 mg/l

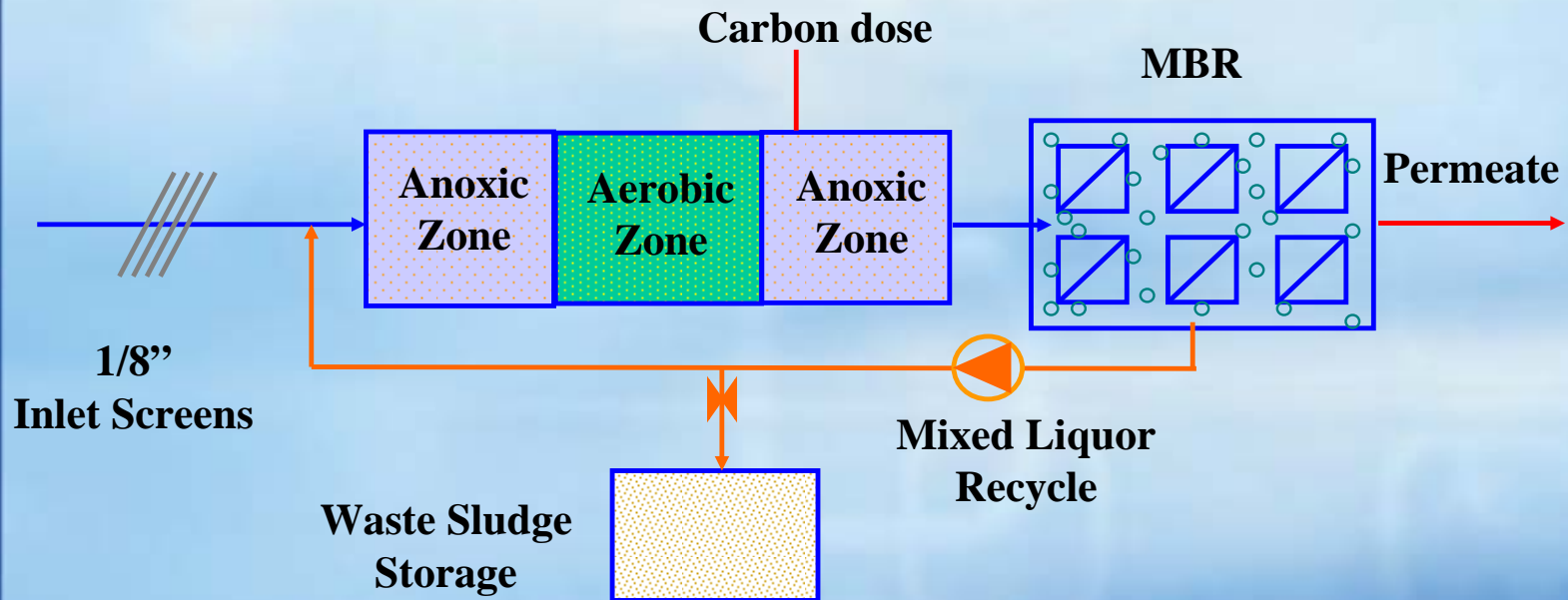


Denitrification by recirculation



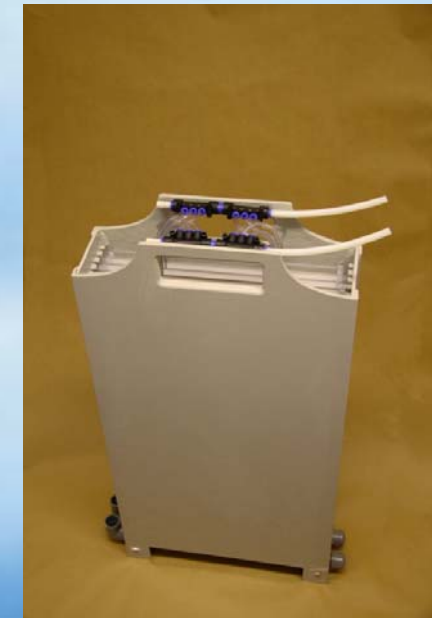
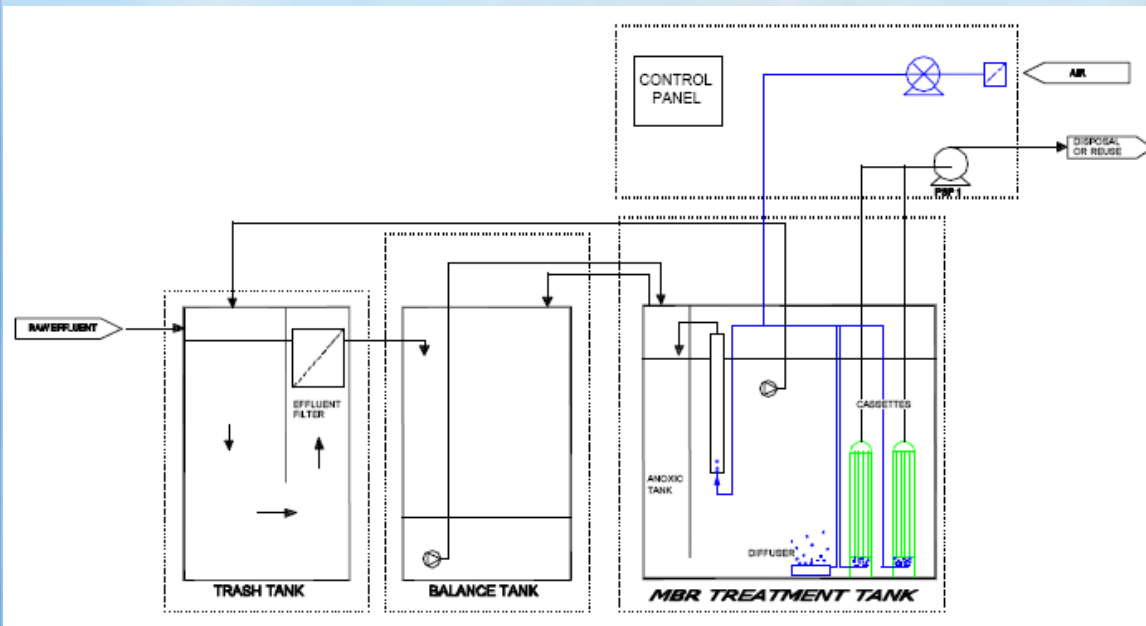
Denitrification by recirc & carbon dose anoxic stages

Design for TN removal < 5 mg/l



Compact Membrane

- Membrane for flows from 500 to 5000 gpd
- Integral or separate septic & equalization tank arrangements



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Membrane Bio Reactors

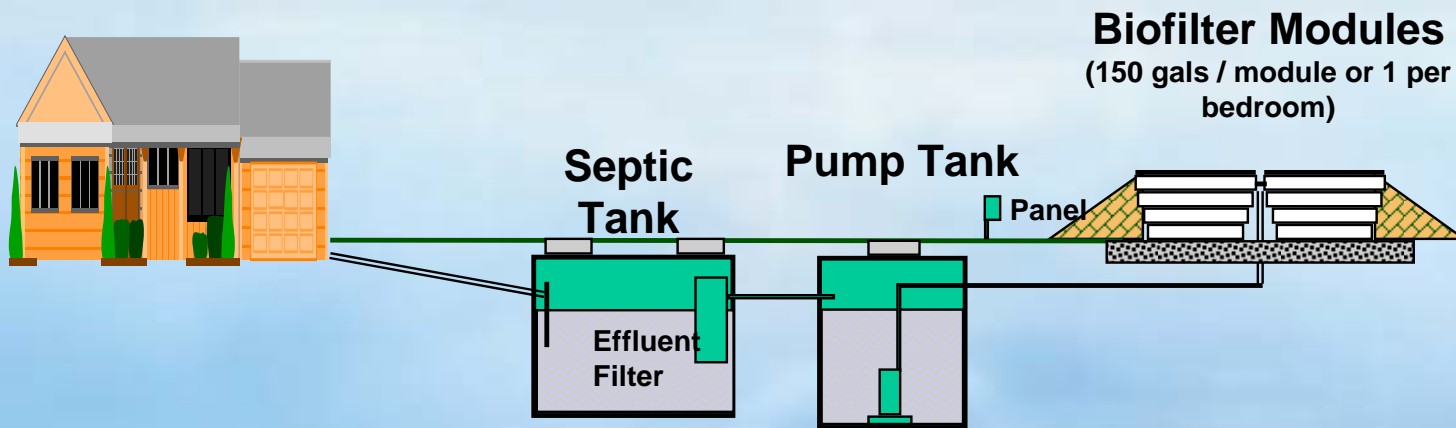
- **Advantages include**
 - Can provide the highest effluent quality when properly designed. Membrane systems are often chosen where a BOD of less than 5 mg/l is combined with total nitrogen levels of less than 10 mg/l.
 - Small footprint area.
 - Long solids retention times can be achieved allowing slow growing nitrifiers to establish
 - Cost effective where strict ammonia and total nitrogen standards are required
- **Limitations**
 - MBR systems may have higher energy costs
 - A higher degree of operational input may be required
 - The anoxic tank needs to be designed for the relatively high levels of DO in the mixed liquor recycle

Media Biofilters

Include

- **Peat**
- **Textile**
- **Sand**
- **Coir**
- **Foam**

Peat Biofilter



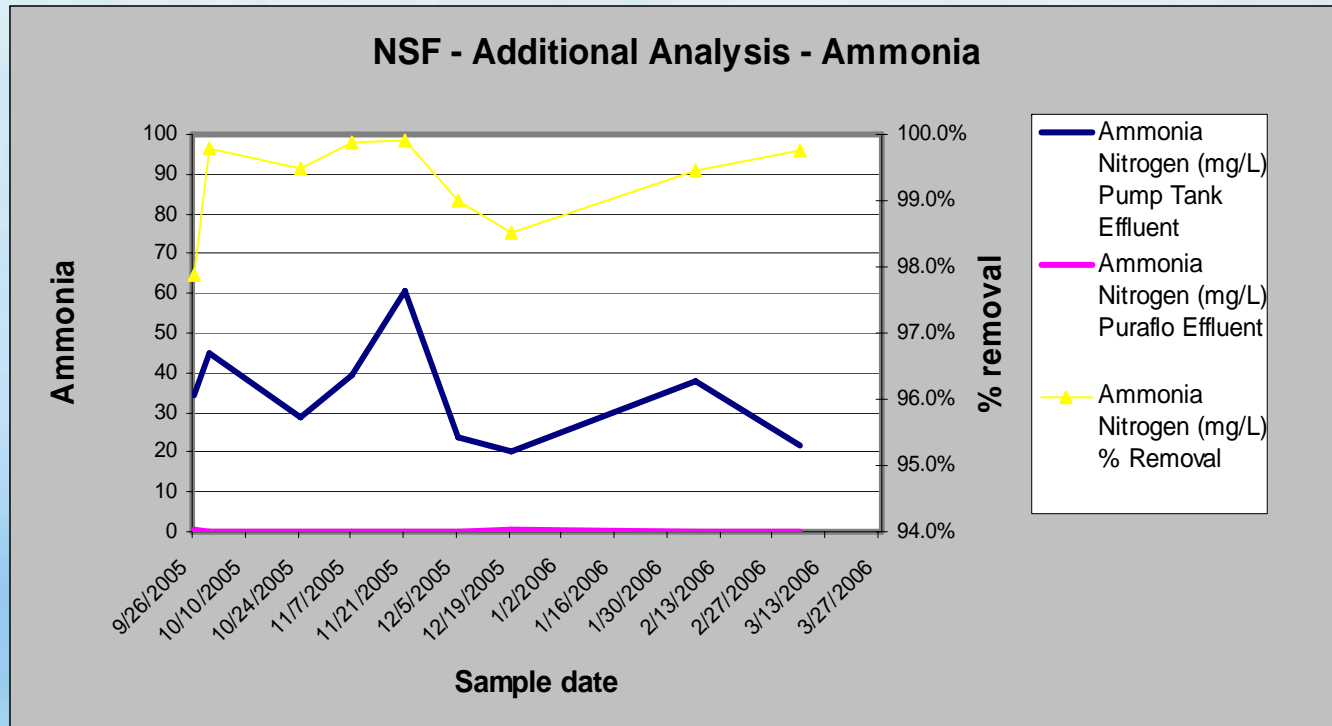
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Puraflo® Peat Biofilter Performance

Parameter	Effluent	NSF Certified	%
BOD (mg/L)	<10	<2	96+
TSS (mg/L)	<10	<2	95+
NH ₃ -N (mg/L)	< 5	<1	90+
Fecal Coliforms (cfu/100 ml)	6000	3000*	99.9+
Total Nitrogen**	<10		

- *GEOMEAN
- ** WITH POST ANOXIC TANK

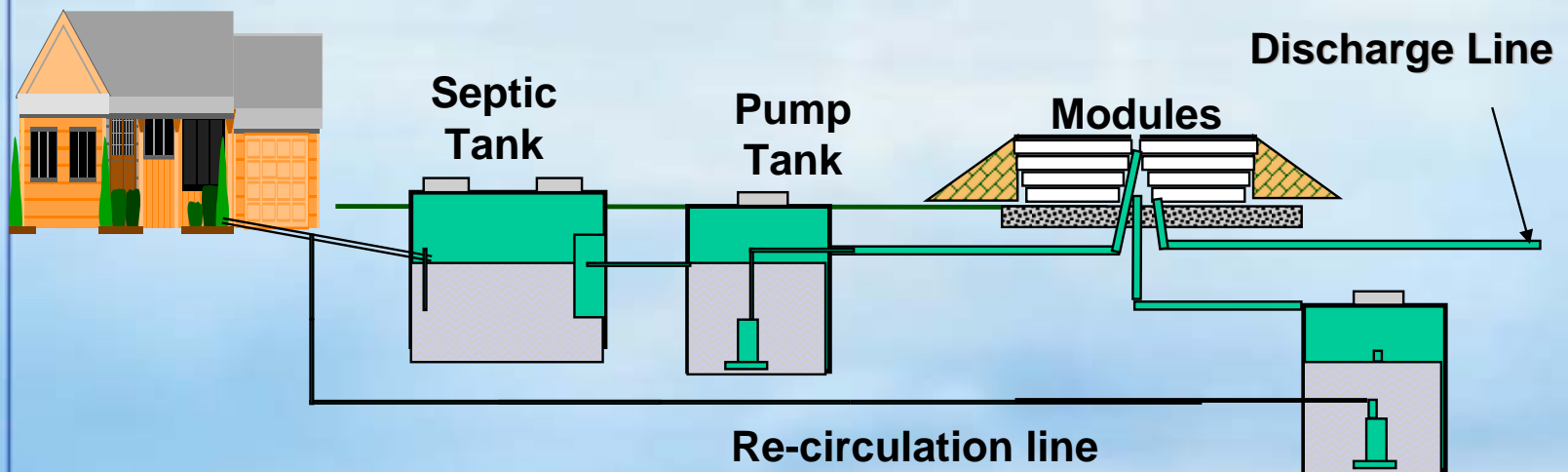
A proportion of remaining nitrogen will be absorbed through the soil / root systems



09/26/05	09/30/05	10/24/05	11/07/05	11/21/05	12/05/05	12/19/06	01/16/06	02/06/06	03/06/06
0.73	0.09	0.15	0.05	0.05	0.24	0.3	0.08	0.21	0.05

Nitrification occurs in the lower section of the media where the BOD level is lower allowing the nitrifiers to compete with the heterotrophic bacteria

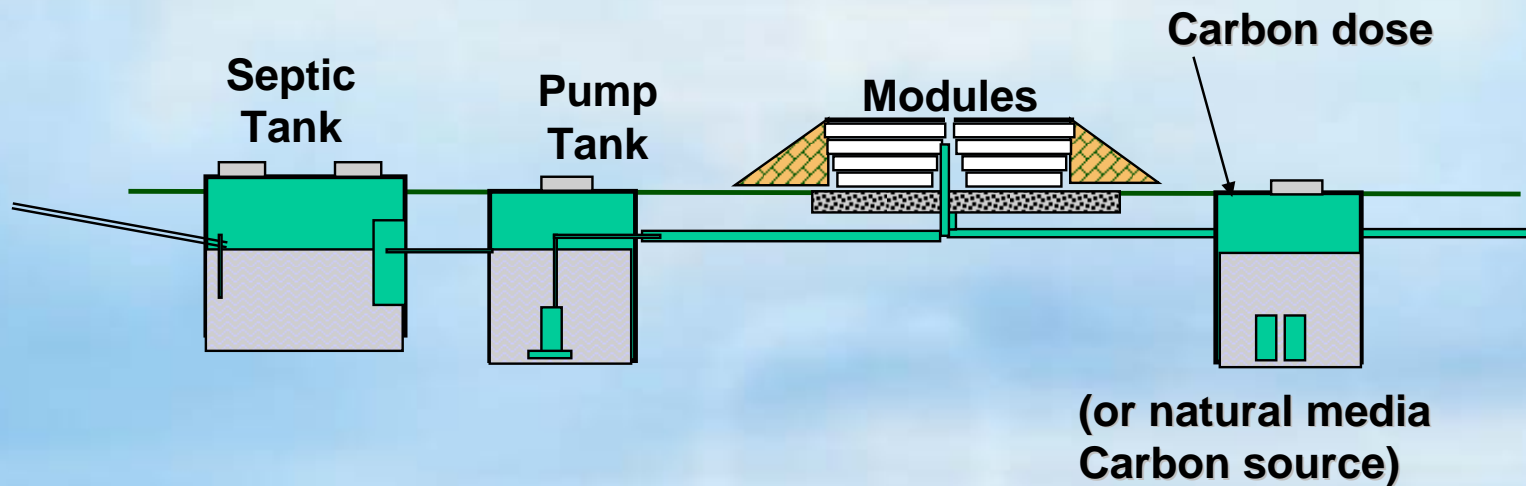
Puraflo[®] Nutrient Reduction



- **30% Nitrogen reduction in single pass time dosed system**
- **50 to 70% Total Nitrogen reduction achieved by recirculating half to one times the design flow back to the septic tank**

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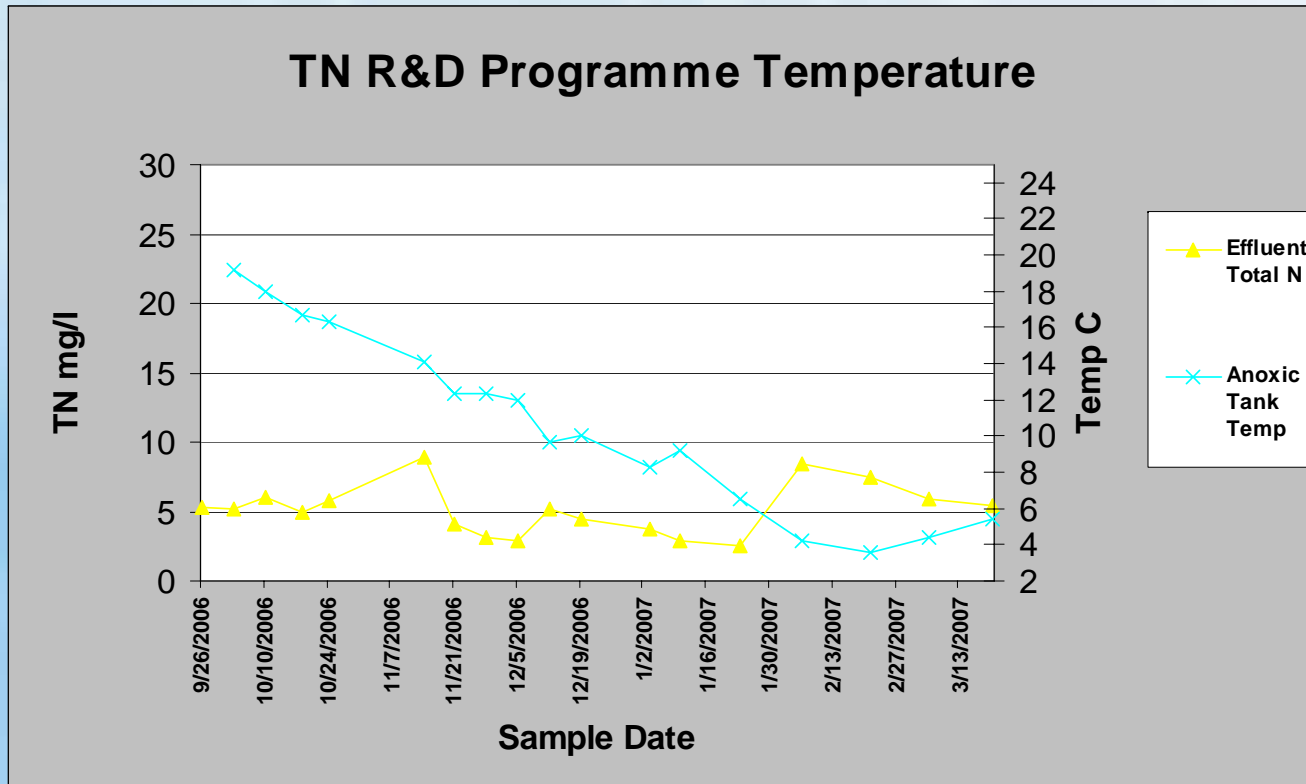
Puraflo[®] Nutrient Reduction



- **<10 mg/l Total Nitrogen with post anoxic tank**

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3rd Party Winter Testing



Third party testing results

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Peat media biofilters

- **Advantages include**
 - Naturally nitrifies making the systems attractive for ammonia standards
 - Standard design incorporates flow equalization and time dosing
 - Excellent for intermittent flows
 - Low operational and maintenance requirements
- **Limitations**
 - The footprint size is relatively large
 - A post anoxic reactor may require re-oxygenation of the effluent where discharging to a surface water
 - For on-site systems a non-toxic carbon source would be required. There are a number of chemicals commercially available.

Conclusions

- **The choice of technology is driven by**
 - the regulatory permit standards and assessment of influent load
 - the cost of the systems that can achieve the standards
 - the risk approach the manufacturers take in proposing a technology
- **On-site & decentralized plants suffer from wide variations in the influent TKN concentrations, large flow variations and a lack of operational attendance to adjust the plant to the conditions experienced - > need for robust process design for small flows**
- **Grab samples based on absolute effluent standards require equalization of flows**
- **Options to achieve a % reduction & reduce risk of low alkalinity**
 - Recirculation 0.5 to 6 x design flow – 50 to 90% reduction of TN
- **Options <10 mg/l, high strength or potential carbon deficiency**
 - Post anoxic tank with carbon dosing (Micro C) or natural carbon media eg wood chips
 - Use recirculation & post anoxic
 - Membranes for tight effluent standards